Pt. 63, Subpt. FFFF, Table 4

And you must . . .

Not applicable.

Not applicable.

Environmental Protection Agency

Then you must . . .

1. Process with Group 1 batch process vents.

For each . . .

a. Reduce collective uncontrolled organic HAP emissions from the sum of all batch process vents within the process by ≥98 percent by weight by venting emissions from a sufficient number of the vents through one or more closed-vent systems to any combination of

- control devices (except a flare); or b. Reduce collective uncontrolled organic HAP emissions from the sum of all batch process vents within the process by ≥95 percent by weight by venting emissions from a sufficient number of the vents through one or more closed-vent systems to any combination of re-covery devices or a biofilter, except you may elect to comply with the requirements of subpart WW of this part for any process tank; or c. Reduce uncontrolled organic HAP emissions
- from one or more batch process vents within the process by venting through a closed-vent system to a flare or by venting through one or more closed-vent systems to any combination of control devices (excluding a flare) that reduce organic HAP to an outlet concentration ≤20 ppmv as TOC or total organic HAP. a. Use a halogen reduction device after the com-

bustion control device; or

For all other batch process vents within the process, reduce collective organic HAP emissions as specified in item 1.a and/or item 1.b of this

2. Halogenated Group 1 batch process vent for which you use a combustion device to control organic HAP emis-

sions.

b. Use a halogen reduction device before the

- i. Reduce overall emissions of hydrogen halide and halogen HAP by ≥99 percent; or
- ii. Reduce overall emissions of hydrogen halide and halogen HAP to ≤0.45 kg/hr; or
- iii. Reduce overall emissions of hydrogen halide and halogen HAP to a concentration ≤20 ymag Reduce the halogen atom mass emission rate to

≤0.45 kg/hr or to a concentration ≤20 ppmv.

combustion control device. [68 FR 63888, Nov. 10, 2003, as amended at 71 FR 40339, July 14, 2006]

TABLE 3 TO SUBPART FFFF OF PART 63—EMISSION LIMITS FOR HYDROGEN HALIDE AND HALOGEN HAP EMISSIONS OR HAP METALS EMISSIONS FROM PROCESS VENTS

As required in §63.2465, you must meet each emission limit in the following table that applies to your process vents that contain hydrogen halide and halogen HAP emissions or PM HAP emissions:

For each	You must
Process with uncontrolled hydrogen halide and halogen HAP emissions from process vents ≥1,000 lb/yr.	a. Reduce collective hydrogen halide and halogen HAP emissions by ≥99 percent by weight or to an outlet concentration ≤20 ppmv by venting through one or more closed-vent systems to any combination of control devices, or
	b. Reduce the halogen atom mass emission rate from the sum of all batch process vents and each individual continuous process vent to ≤0.45 kg/hr by venting through one or more closed-vent systems to a halogen reduction device.
 Process at a new source with uncontrolled emissions from process vents ≥150 lb/ yr of HAP metals. 	Reduce overall emissions of HAP metals by ≥97 percent by weight.

[68 FR 63888, Nov. 10, 2003, as amended at 71 FR 40340, July 14, 2006]

TABLE 4 TO SUBPART FFFF OF PART 63—EMISSION LIMITS FOR STORAGE TANKS

As required in §63.2470, you must meet each emission limit in the following table that applies to your storage tanks:

For each	For which	Then you must
1. Group 1 storage tank	a. The maximum true vapor pressure of total HAP at the storage temperature is ≥76.6 kilopascals.	i. Reduce total HAP emissions by ≥95 percent by weight or to ≤20 ppmv of TOC or organic HAP and ≤20 ppmv of hydrogen halide and halogen HAP by venting emissions through a closed vent system to any combination of control devices (excluding a flare); or

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For each	For which	Then you must
		ii. Reduce total organic HAP emissions by venting emissions through a closed vent system to a flare; or iii. Reduce total HAP emissions by venting emissions to a fuel gas system or process in accordance with §63.982(d) and the requirements referenced therein.
	b. The maximum true vapor pressure of total HAP at the stor- age temperature is <76.6 kilopascals.	i. Comply with the requirements of subpart WW of this part, except as specified in § 63.2470; or
	·	ii. Reduce total HAP emissions by ≥95 percent by weight or to ≤20 ppmv of TOC or organic HAP and ≤20 ppmv of hydrogen halide and halogen HAP by venting emissions through a closed vent system to any combination of control devices (excluding a flare); or iii. Reduce total organic HAP emissions by venting emissions through a
		closed vent system to a flare; or
		iv. Reduce total HAP emissions by venting emissions to a fuel gas system or process in accordance with §63.982(d) and the requirements referenced therein.
Halogenated vent stream from a Group 1 storage tank.	You use a combustion control device to control organic HAP emissions.	Meet one of the emission limit options specified in Item 2.a.i or ii. in Table 1 to this subpart.

[68 FR 63888, Nov. 10, 2003, as amended at 71 FR 40340, July 14, 2006]

Table 5 to Subpart FFFF of Part 63—Emission Limits and Work Practice Standards for Transfer Racks

As required in $\S63.2475$, you must meet each emission limit and work practice standard in the following table that applies to your transfer racks:

For each	You must	
1. Group 1 transfer rack	a. Reduce emissions of total organic HAP by ≥98 percent by weight or to an outlet concentration ≤20 ppmv as organic HAP or TOC by venting emissions through a closed-vent system to any combination of control devices (except a flare); or b. Reduce emissions of total organic HAP by venting emissions through a closed-vent system to a flare; or	
	c. Reduce emissions of total organic HAP by venting emissions to a fuel gas system or process in accordance with §63.982(d) and the requirements referenced therein; or	
	d. Use a vapor balancing system designed and operated to collect organic HAP vapors displaced from tank trucks and railcars during loading and route the collected HAP vapors to the storage tank from which the liquid being loaded originated or to another storage tank connected by a common header.	
Halogenated Group 1 trans- fer rack vent stream for which you use a combustion device to control organic HAP emissions.	 a. Use a halogen reduction device after the combustion device to reduce emissions of hydrogen halide and halogen HAP by ≥99 percent by weight, to ≤0.45 kg/hr, or to ≤20 ppmv; or b. Use a halogen reduction device before the combustion device to reduce the halogen atom mass emission rate to ≤0.45 kg/hr or to a concentration ≤20 ppmv. 	

 $[68 \; \mathrm{FR} \; 63888, \; \mathrm{Nov.} \; 10, \; 2003, \; \mathrm{as} \; \mathrm{amended} \; \mathrm{at} \; 71 \; \mathrm{FR} \; 40341, \; \mathrm{July} \; 14, \; 2006]$

Table 6 to Subpart FFFF of Part 63—Requirements for Equipment Leaks

As required in 63.2480, you must meet each requirement in the following table that applies to your equipment leaks:

For all	And that is part of	You must
Equipment that is in organic HAP service.	a. Comply with the requirements of subpart UU of this part 63 and the requirements referenced therein, except as specified in § 63.2480(b) and (d); or.	