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the flow meter data using the manufacturer's prescribed method.

(ii) Calculate values of the calibration coefficient for each test point:

$$K_v = \frac{Q_s \sqrt{T_v}}{P_v}$$

Q<sub>s</sub>=Flow rate in standard cubic meter per minute, at the standard conditions of 20 °C, 101.3 kPa.

T<sub>v</sub>=Temperature at venturi inlet, °K.

P<sub>v</sub>=Pressure at venturi inlet, kPa

=P<sub>B</sub> - P<sub>Pi</sub>

Where:

P<sub>Pi</sub> = Venturi inlet pressure depression, kPa.

(iii) Plot K<sub>v</sub> as a function of venturi inlet pressure. For choked flow, K<sub>v</sub> will have a relatively constant value. As pressure decreases (vacuum increases), the venturi becomes unchoked and K<sub>v</sub> decreases. (See Figure 7 in appendix B of this subpart)

(iv) For a minimum of eight points in the critical region calculate an average K<sub>v</sub> and the standard deviation.

(v) If the standard deviation exceeds 0.3 percent of the average K<sub>v</sub>, take corrective action.

(e) CVS system verification. The following "gravimetric" technique can be used to verify that the CVS and analytical instruments can accurately measure a mass of gas that has been injected into the system. (Verification can also be accomplished by constant flow metering using critical flow orifice devices.)

(1) Obtain a small cylinder that has been charged with 99.5 percent or greater propane or carbon monoxide gas (CAUTION—carbon monoxide is poisonous).

(2) Determine a reference cylinder weight to the nearest 0.01 grams.

(3) Operate the CVS in the normal manner and release a quantity of pure propane into the system during the sampling period (approximately five minutes).

(4) The calculations are performed in the normal way except in the case of propane. The density of propane (0.6109 kg/m<sup>3</sup>carbon atom is used in place of the density of exhaust hydrocarbons.

(5) The gravimetric mass is subtracted from the CVS measured mass and then divided by the gravimetric

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mass to determine the percent accuracy of the system.

(6) Good engineering practice requires that the cause for any discrepancy greater than ±2 percent must be found and corrected.

**§91.425 CVS calibration frequency.**

Calibrate the CVS positive displacement pump or critical flow venturi following initial installation, major maintenance or as necessary when indicated by the CVS system verification (described in §91.424(e)).

**§91.426 Dilute emission sampling calculations.**

(a) The final reported emission test results must be computed by use of the following formula:

$$A_{wm} = \frac{\sum(W_i \times f_i)}{\sum(P_i \times f_i)} \times K_{Hi}$$

Where:

A<sub>wm</sub>=Weighted mass emission level (HC, CO, CO<sub>2</sub>, or NO<sub>x</sub>) for a test [g/kW-hr].

W<sub>i</sub>=Average mass flow rate of an emission from a test engine during mode i [g/hr].

WF<sub>i</sub> = Weighting factor for each mode i as defined in §91.410(a).

P<sub>i</sub> = Gross average power generated during mode i [kW] calculated from the following equation (power for the idle mode shall always be zero for this calculation):

$$P_i = \frac{2 \Pi}{60,000} \times \text{speed} \times \text{torque}$$

speed = average engine speed measured during mode i [rev./minute]

torque = average engine torque measured during mode i [N-m]

K<sub>Hi</sub> = Humidity correction factor for mode i. This correction factor only affects calculations for NO<sub>x</sub> and is equal to one for all other emissions. K<sub>Hi</sub> is also equal to one for all two-stroke engines.

(b) The mass flow rate (W<sub>i</sub>) of an emission for mode i is determined from the following equation:

$$W_i = Q_i \times D \times \left( C_{Di} - C_{Bi} \times \left( 1 - \frac{1}{DF_i} \right) \right)$$

Where:

Q<sub>i</sub> = Volumetric flow rate of the dilute exhaust through the CVS at standard conditions [m<sup>3</sup>/hr at STP].

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D = Density of a specific emission ( $D_{HC}$ ,  $D_{CO}$ ,  $D_{CO_2}$ ,  $D_{NO_x}$ ) in the exhaust [ $g/m^3$ ].

$DF_i$  = Dilution factor of the dilute exhaust during mode i.

$C_{Di}$  = Concentration of the emission (HC, CO,  $NO_x$ ) in the dilute exhaust extracted from the CVS during mode i [ppm].

$C_{Bi}$  = Concentration of the emission (HC, CO,  $NO_x$ ) in the background sample during mode i [ppm].

STP = Standard temperature and pressure. All volumetric calculations made for the equations in this section are to be corrected to a standard temperature of 20 °C and 101.3 kPa.

(c) Densities for emissions that are to be measured for this test procedure are:

$$\begin{aligned} D_{HC} &= 576.8 \text{ g/m}^3 \\ D_{NO_x} &= 1912 \text{ g/m}^3 \\ D_{CO} &= 1164 \text{ g/m}^3 \\ D_{CO_2} &= 1829 \text{ g/m}^3 \end{aligned}$$

(1) The value of  $D_{HC}$  above is calculated based on the assumption that the fuel used has a carbon to hydrogen ratio of 1:1.85. For other fuels,  $D_{HC}$  can be calculated from the following formula:

$$D_{HC} = \frac{M_{HC}}{R_{STP}}$$

Where:

$M_{HC}$  = Molecular weight of the hydrocarbon molecule divided by the number of carbon atoms in the molecule [ $g/mole$ ].

$R_{STP}$  = Ideal gas constant for a gas at STP = 0.024065 [ $m^3 \cdot mole$ ].

(2) The idealized molecular weight of the exhaust hydrocarbons, ie., the molecular weight of the hydrocarbon molecule divided by the number of carbon atoms in the molecule,  $M_{HC}$  can be calculated from the following formula:

$$M_{HC} = M_C + \alpha M_H + \beta M_O$$

Where:

$M_C$  = Molecular weight of carbon = 12.01 [ $g/mole$ ].

$M_H$  = Molecular weight of hydrogen = 1.008 [ $g/mole$ ].

$\alpha$  = Hydrogen to carbon ratio of the test fuel.

(3) The value of  $D_{NO_x}$  above assumes that  $NO_x$  in entirely in the form of  $NO_2$ .

(d) The dilution factor (DF) is the ratio of the volumetric flow rate of the background air to that of the raw engine exhaust. The following formula is used to determine DF:

$$DF = \frac{13.4}{C_{D_{HC}} + C_{D_{CO}} + C_{D_{CO_2}}}$$

Where:

$C_{D_{HC}}$  = Concentration of HC in the dilute sample [ppm].

$C_{D_{CO}}$  = Concentration of CO in the dilute sample [ppm].

$C_{D_{CO_2}}$  = Concentration of  $CO_2$  in the dilute sample [ppm].

(e) The humidity correction factor  $K_H$  is an adjustment made to the measured  $NO_x$ . This corrects for the sensitivity that a spark-ignition engine has to the humidity of its combustion air. The following formula is used to determine  $K_H$  for  $NO_x$  calculations:

$$K_H = \frac{1}{1 - 0.0329(H - 10.71)}$$

Where:

H = Absolute humidity of the engine intake air [grams of water per kilogram of dry air].

(f) The absolute humidity of the engine intake air H is calculated using the following formula:

$$H = \frac{6.211 P_{dew}}{P_B - \left(\frac{P_{dew}}{100}\right)}$$

Where:

$P_{dew}$  = Saturated vapor pressure at the dew point temperature [kPa].

$P_b$  = Barometric pressure [kPa].

(g) The fuel mass flow rate  $F_i$  can be either measured or calculated using the following formula:

$$F_i = \frac{M_f}{T}$$

Where:

$M_f$  = Mass of fuel consumed by the engine during the mode [g].

T = Duration of the sampling period [hr].

(h) The mass of fuel consumed during the mode sampling period,  $M_{FUEL}$  can be calculated from the following equation:

$$M_f = \frac{G_s}{R_2 \times 273.15}$$

Where:

$G_s$  = Mass of carbon measured during the mode sampling period [g].

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R<sub>2</sub> = The fuel carbon weight fraction, which is the mass of carbon in fuel per mass of fuel [g/g].

(i) The grams of carbon measured during the mode G<sub>s</sub> can be calculated from the following equation:

$$G_s = \frac{12.011 \times HC_{\text{mass}}}{12.011 + 1.008\alpha} + 0.429CO_{\text{mass}} + 0.273CO_{2\text{mass}}$$

Where:

HC<sub>mass</sub> = mass of hydrocarbon emissions for the mode sampling period [g].

CO<sub>mass</sub> = mass of carbon monoxide emissions for the mode sampling period [g].

CO<sub>2mass</sub> = mass of carbon dioxide emissions for the mode sampling period [g].

α = The atomic hydrogen to carbon ratio of the fuel.

**§91.427 Catalyst thermal stress resistance evaluation.**

(a)(1) The purpose of the evaluation procedure specified in this section is to determine the effect of thermal stress on catalyst conversion efficiency. The thermal stress is imposed on the test catalyst by exposing it to quiescent heated air in an oven. The evaluation of the effect of such stress on catalyst performance is based on the resultant degradation of the efficiency with which the conversions of specific pollutants are promoted. The application of this evaluation procedure involves the several steps that are described in the following paragraphs.

(2) The engine manufacturer need not submit catalyst conversion efficiency data for pollutants that the catalyst being tested was not designed to reduce/oxidize. The engine manufacturer must specify the pollutants that the catalyst will be converting and submit catalyst conversion efficiency data on only those pollutants.

(b) Determination of initial conversion efficiency.

(1) A synthetic exhaust gas mixture having the composition specified in §91.329 is heated to a temperature of 450 ±5 °C and passed through the new test catalyst or, optionally, a test catalyst that has been exposed to temperatures less than or equal to 500 °C for less than or equal to two hours, under flow conditions that are representative of anticipated in-use conditions.

(2) The concentration of each pollutant of interest, that is, hydrocarbons, carbon monoxide, or oxides of nitrogen, in the effluent of the catalyst is determined by means of the instrumentation that is specified for exhaust gas analysis in subpart D of this part.

(3) The conversion efficiency for each pollutant is determined by:

(i) Subtracting the effluent concentration from the initial concentration,

(ii) Dividing this result by the initial concentration,

(iii) Multiplying this result by 100 percent.

(c) Imposition of thermal stress.

(1) The catalyst is placed in an oven that has been pre-heated to 1000 °C and the temperature of the air in the oven is maintained at 1000 ±10 °C for six hours. Optionally, the catalyst may instead be placed in an oven having a 90% nitrogen/10% water vapor environment that has been pre-heated to at least 850 °C and the temperature of the nitrogen/water vapor environment in the oven is maintained at 850 °C ±10 °C for six hours.

(2) The catalyst is removed from the oven and allowed to cool to room temperature.

(d) Determination of final conversion efficiency. The steps listed in paragraph (b) of this section are repeated.

(e) Determination of conversion efficiency degradation.

(1) The final conversion efficiency determined in paragraph (c) of this section is subtracted from the initial conversion efficiency determined in paragraph (b) of this section.

(2) This result is divided by the initial conversion efficiency.

(3) This result is multiplied by 100 percent.

(f) Determination of compliance with degradation limit. The percent degradation determined in paragraph (e) of